

Development of High Temperature Membranes and Improved Cathode Catalysts for PEM Fuel Cells



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DoE Agreement DE-FC04C-02-A1-67608 Program Manager – Amy Manheim

Objectives and Approach



Improved Cathode Catalysts

- Goals:
 - To improve power density
 - Lower cost, \$/kW
- Approach:
 - Higher activity cathode catalyst systems: binary and ternary alloys. High loading of noble metal to decrease electrode thickness and achieve mass transport benefit

High Temperature Fundamentals and Membrane Development (100-120 C, 1.0-1.5 atm):

- Goals to improve:
 - Anode and cathode kinetics
 - System heat management
- Approach:
 - Collaboration with leading polymer chemists to develop new membrane systems: poly(arylene ether sulfone), PEEK, multiblock polymers and inorganic solid conductor filled Nafion®
 - Fundamental understanding of HT operation limitations and possible solutions through modeling and experimental work

Technical Barriers, Budget, Team



Technical Barriers

- P. Durability
- Q. Electrode Performance
- R. Thermal and Water Management

Budget

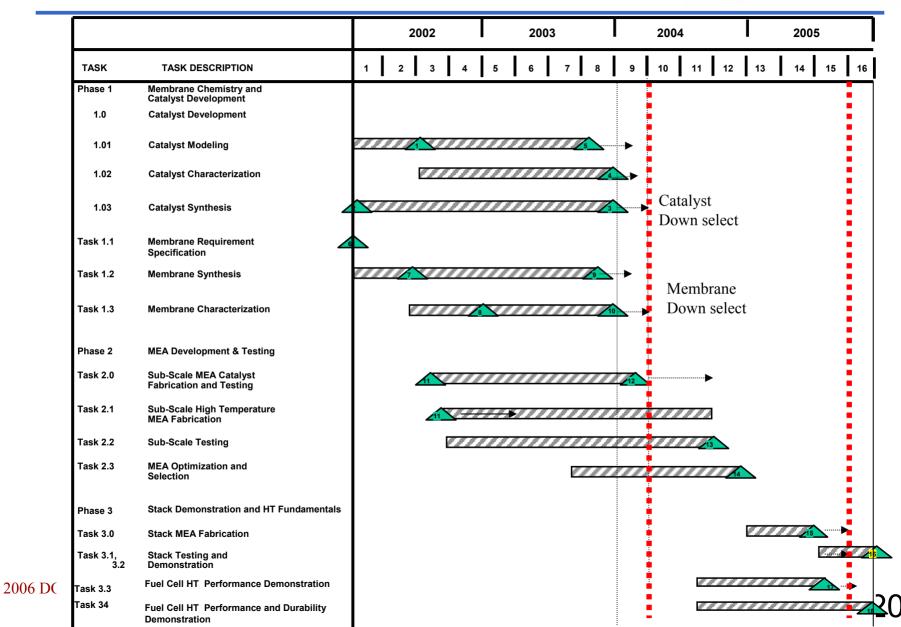
Year	Total \$M	DoE \$M	UTC \$M
Overall 2002-2005	9.500	7.600	1.900
Received in 2005	1.875	1.500	.375

Program Team at Closing

- <u>UTC Power</u> (Dr. L.Protsailo): general coordination, catalyst development, modeling, fuel cell testing, fundamentals and stack development
- <u>UTRC</u> (Dr. N.Cipollini): MEA optimization and fabrication
- <u>VaTech</u> (Prof. J. McGrath): membrane development, fundamentals of membrane architecture
- <u>UCONN</u> (Prof. J.Fenton): membrane development, MEA fabrication, HT fundamentals

Program Schedule





Membrane Development Approach



VaTech approach – sulfonated biphenole-sulfones

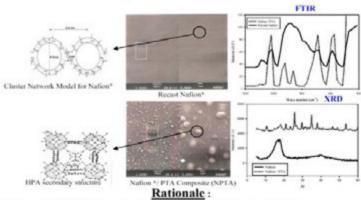
Acronym: BPSH-XX Bi

Phenol Sulfone: H Form

Good mechanical and thermal properties (T_g>>120°C), monomers commercially available (low cost)

<u>UCONN approach</u> – composite membranes based on Nafion® and solid proton conductor – retain conductivity at low RH%

Nafion®/Heteropolyacid Composite Membranes



- Inherently high HPA conductivity at high humidities (~ 0.2 S/cm)
- Induction of alternate conduction mechanisms i.e. enhancement of proton hopping



2 different approaches for HT membrane development were investigated under this program:

- Approach A
 - First generation: Series II solid acid doped reinforced Nafion-like membrane
 - Nafion®-Teflon®phosphotungstic acid (NTPA) (Na-form)- Series II membrane
 - Second generation: Series IV Cs form in-situ doped reinforced Nafion-like membrane

<u>UCONN</u>

- Approach B
 - First generation: BPSH-XX

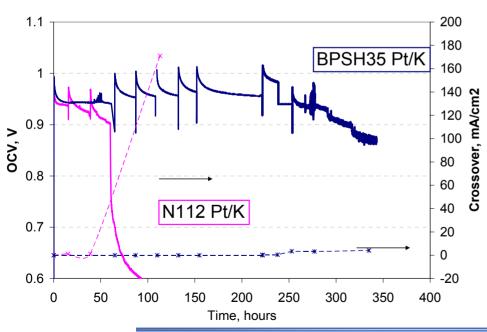
- Second generation: BPSH-XX with high molecular weight, partially fluorinated, increased acidity of functional group
- Third generation: multiblock copolymers

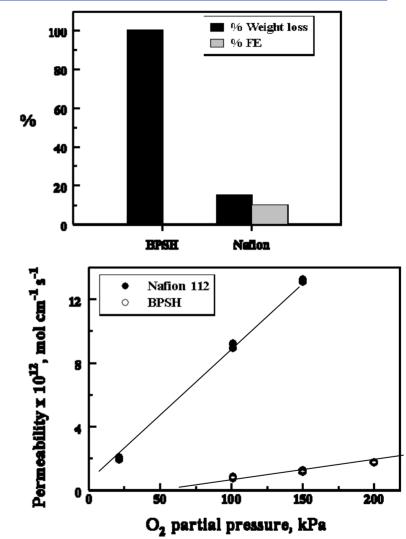
VaTech



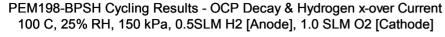
Chemical Stability in OCV Test

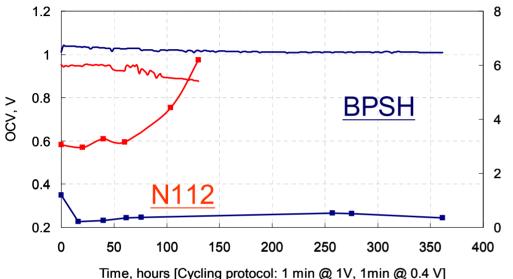
- 1. Fails Fenton test
- 2. Low O_2 permeability
- 3. Outstanding durability at OCV hold conditions











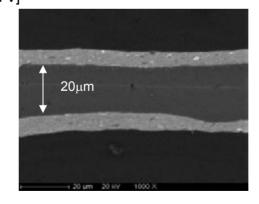
Load Cycle Test

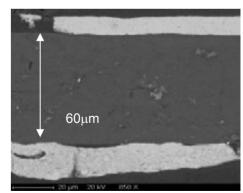
Load cycle protocol:

- 100°C, 25%RH
- 0.5 SLPM H₂/1.0 SLPM O₂
- 1min @ 1V, 1min @ 0.4V

EMPA post test analysis:

 BPSH retained its thickness in load cycle test





Nafion® 112

BPSH-37

2006 DOE Hydrogen Program Review May 13-16, 2006 Arlington, VA

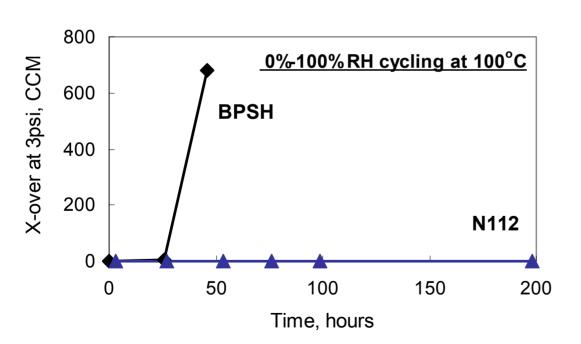
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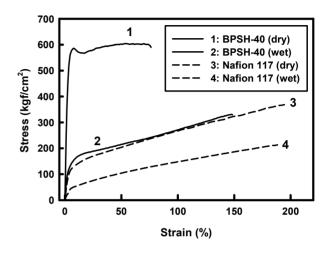
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RH Cycle Test

Membrane	Linear expansion x- direction, %	Linear expansion y- direction, %	Swelling (boiling), %
BPSH	25	15	41.2
N112	10	3.1	11.4

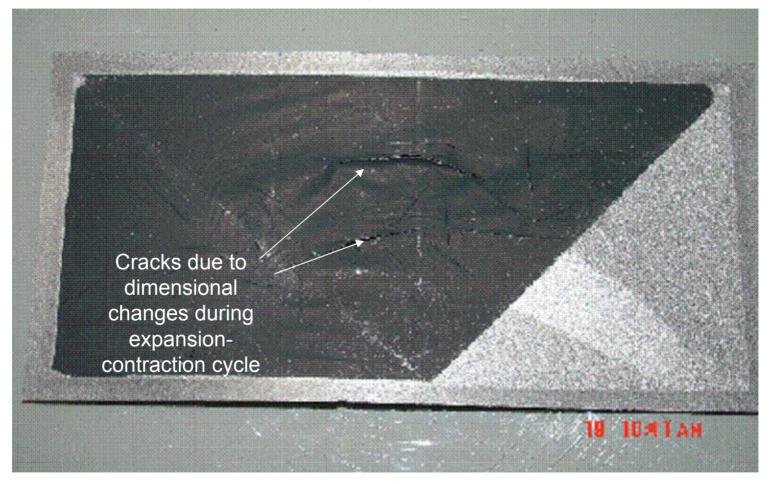








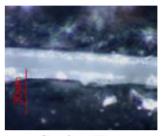
Unitized Electrode Assembly



Technical Accomplishments: NTPA-Cs Membrane



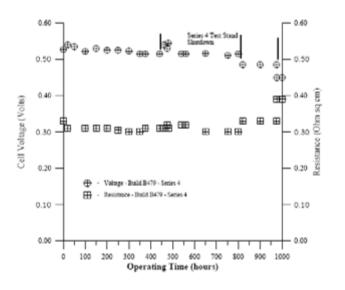
- Composite membranes based on Nafion® and solid proton conductor retain conductivity at low RH%
 - Nafion®-Teflon®-phosphotungstic acid (NTPA) (Na-form)- Series II membrane
 - Nafion®-Teflon®-phosphotungstic acid (NTPA) (Cs-form) Series IV membrane
 - · Smaller uniform particle size
 - Solid acid proton conductor is precipitated in-situ
 - Cs-form is insoluble
 - Processed at higher T°C
 - durability +

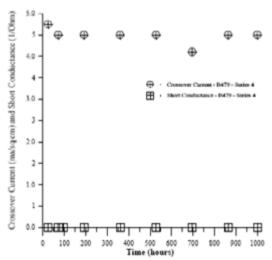




Series II

Series IV





1000 hrs demonstrated at 100°C, 25%RH;

No membrane failure observed @ 1000 hours

HT/Low RH Operation Modeling

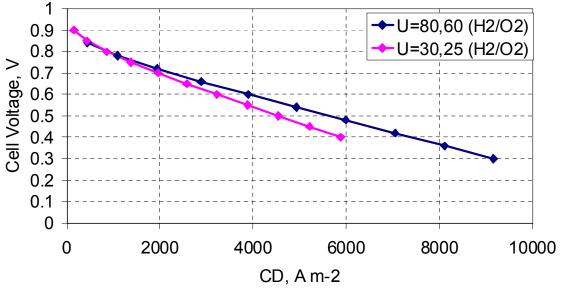


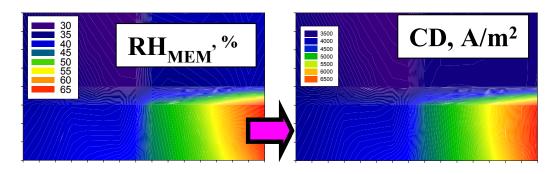
- Performance improves at higher utilizations
 - RH&Conductivity
 DOMINATE
 PERFORMANCE over O₂
 concentration

Performance Curves 100 C, 25% RH, 150 kPa, 0.9 8.0 0.7 U[H2/AIR] = 80,60Voltage, V 5.0 6.0 7.0 U[H2/AIR1 = 30.25 0.3 0.2 0.1 0 100 200 300 400 500 600

Current Density, mA/cm2

Performance Simulations H2/Air, 100 C, 25% RH, 150 kPa Nafion 112

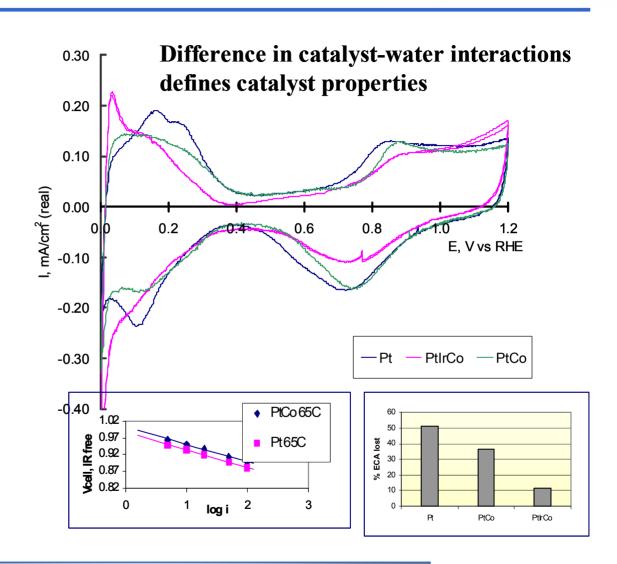




Cathode Catalyst Development Approach

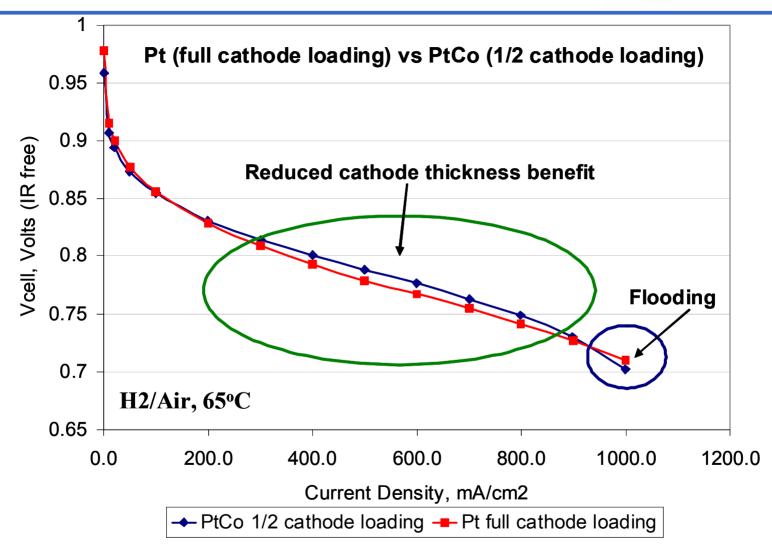


- Higher activity cathode catalyst systems: binary and ternary alloys
 - Carbothermal synthesis
 - PtCo and PtIrCo leading systems
- High loading of noble metal to decrease electrode thickness and achieve mass transport benefit



MEA Optimization





PtCo 20-Cell Stack



PtCo 20-cell stack was delivered to ANL for durability studies. Technical support is provided.

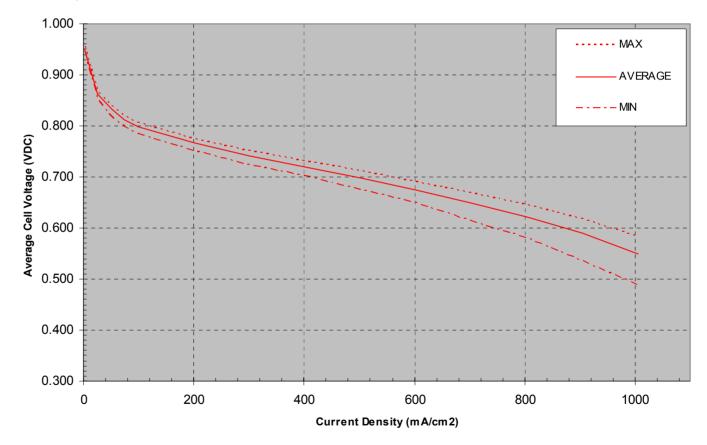
PtCo MEA specification:

0.35mgPt/cm²

Nafion® 112

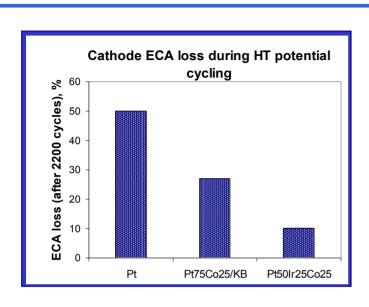
Toray GDL

UTCFC planform (400cm²)



Alloy Catalyst Durability





Potential cycling conditions:

120°C, 50%RH;

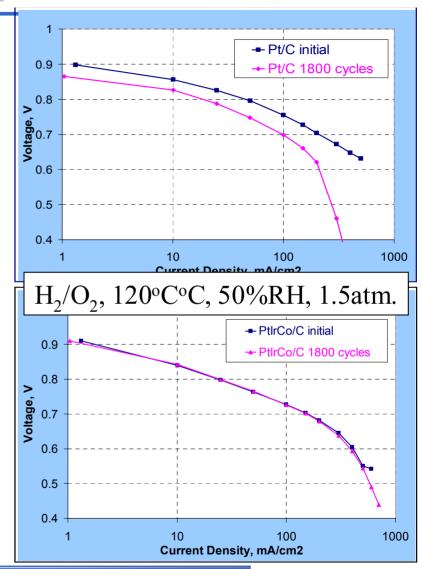
2800 cycles; H_2/N_2 30s 0.87-30s 1.05V

Pt/C: ~ 45% ECA decrease; 25mV

performance loss

PtIrCo/C: ~ 6% ECA decrease; 3mV

performance loss



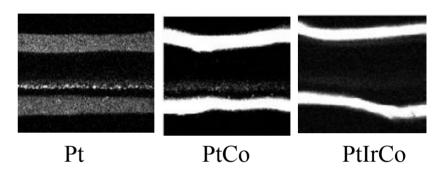
Alloy Effect on Ionomer Durability



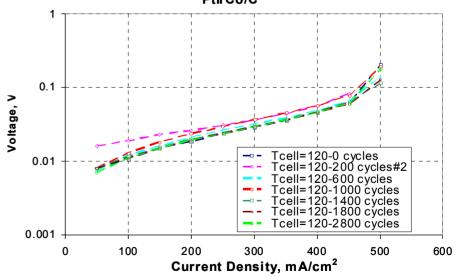
- $-10 \% H_2$ in N_2 , low utilization
- Electrode Ionic resistance changes with time
- PtIrCo cathode prevents ionomer poisoning

H2 Pump ELECTRODE RESISTANCE Pt/C ELECTRODE RESISTANCE, Tcell=120-0 cycles 0.01 Tcell=120-600 cycles#1 Tcell=120-1000 cycles#1 Tcell=120-1400 cycles#1 Tcell=120-1800 cycles#1 Tcell=120-2200 cycles#1 0.001 0 100 200 300 400 500 Current Density, mA/cm2

Pt EMPA map after cycling



H2 Pump ELECTRODE RESISTANCE Curves PtirCo/C







2002 - 2005

- Established the importance of cyclic durability
- Developed best in class PtIrCo alloy catalyst and demonstrated 5x cyclic durability improvement vs. Pt
- Established membrane down-select criteria
- Developed fundamental understanding of hydrocarbon membrane durability
- Demonstrated 1000 hours of operation at 100°C, 25%RH

Responses to Previous Year Reviewers' Comments



- Q1. Shows results on hydrogen/oxygen primarily
 - Initial stages of alloy work were dedicated to activity investigations (thus oxygen data are more useful). MEA optimization step operated with H2/air performance
- Q2. Membrane durability studies weak the new materials are interesting, but durability data are limiting
 - Significant emphasis has been put on fundamental analysis and understanding of alternative membrane durability – especially hydrocarbon membranes
- Q3. Testing of new catalysts in full-size cells and a stack to compliment fundamental studies of catalyst and membrane durability is needed
 - PtCo catalyst was tested in full size cell and 20-cell stack was built and delivered for testing to ANL facilities
 - Attempt to test hydrocarbon membrane in full size cell was made. Unitizing BPSH for full-size testing is a challenging task due to dimensional instability of the membrane.

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